

Introduction to unsteady state heat transfer

Unsteady state heat conduction in various geometries

A general situation is considered where the internal resistance is not small (unlike the lumped parameter model) and the temperature in the solid is not constant

- In the first case, the surface convective resistance is negligible compared to the internal resistance
- This is possible due to very large surface heat transfer coefficient or large conductive resistance in the object
- Unsteady state conduction in the x – *direction* only in a flat plate of thickness $2H$
- The initial temperature profile in the plate at $t = 0$ is uniform at $T = T_o$
- At time $t = 0$, the ambient temperature is suddenly changed to T_1 and held there
- As there is no convective heat transfer resistance, the temperature of the surface is held constant at T_1
- Since conduction is only in the x -direction,

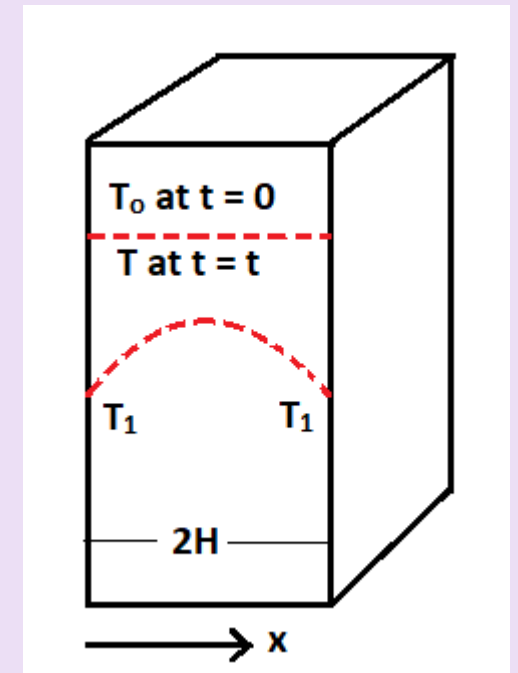
$$\frac{\partial T}{\partial t} = \alpha \frac{\partial^2 T}{\partial x^2}$$

- The initial and boundary conditions are:

$$T = T_o , \quad t = 0 \quad x = x \text{ (at all } x)$$

$$T = T_1 , \quad t = t \quad x = 0$$

$$T = T_1 , \quad t = t \quad x = 2H$$



It is often more convenient to define a dimensionless temperature Y , so it varies between 0 and 1

Hence,

$$Y = \frac{T_1 - T}{T_1 - T_o}$$

Substituting this we get,

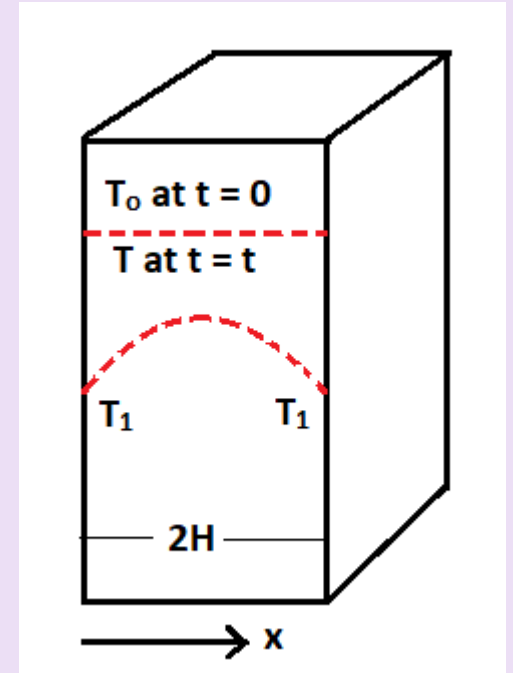
$$\frac{\partial Y}{\partial t} = \alpha \frac{\partial^2 Y}{\partial x^2}$$

Redefining the initial and boundary conditions we get:

$$Y = \frac{T_1 - T_o}{T_1 - T_o} = 1, \quad t = 0 \quad x = x \text{ (at all } x)$$

$$Y = \frac{T_1 - T_1}{T_1 - T_o} = 0, \quad t = t \quad x = 0$$

$$Y = \frac{T_1 - T_1}{T_1 - T_o} = 0, \quad t = t \quad x = 2H$$



The solution to the above equation is ,

$$Y = e^{-a^2 \alpha t} (A \cos ax + B \sin ax)$$

A and B are constants, a is a parameter

Applying the initial and boundary conditions, the final solution to the above equation is an infinite Fourier series

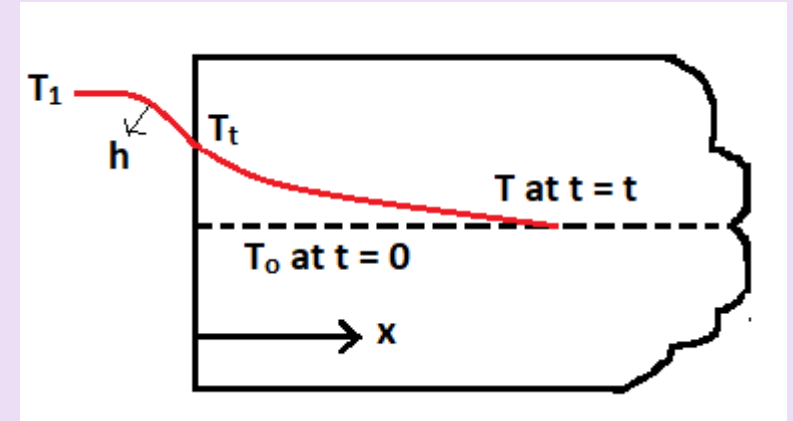
$$\frac{T_1 - T}{T_1 - T_o} = \frac{4}{\pi} \left(\frac{1}{1} \exp \frac{-1^2 \pi^2 \alpha t}{4H^2} \sin \frac{1\pi x}{2H} + \frac{1}{3} \exp \frac{-3^2 \pi^2 \alpha t}{4H^2} \sin \frac{3\pi x}{2H} + \frac{1}{5} \exp \frac{-5^2 \pi^2 \alpha t}{4H^2} \sin \frac{5\pi x}{2H} + \dots \right)$$

The temperature T at any position x and time t can be determined

These equations are very time-consuming to use and convenient charts have been prepared for different applications

Unsteady state heat conduction in a semi-infinite solid

- A semi-infinite solid extends to ∞ in the x – *direction* and heat conduction occurs only in the x – *direction*
- The temperature in the solid is uniform at T_o
- At time $t = 0$, the solid is suddenly exposed to or immersed in a large mass of ambient fluid at a temperature of T_1
- The solution to the differential equation under these conditions is



$$\frac{T - T_o}{T_1 - T_o} = 1 - Y = \operatorname{erfc} \frac{x}{2\sqrt{\alpha t}} - \exp \left[\frac{h\sqrt{\alpha t}}{k} \left(\frac{x}{\sqrt{\alpha t}} + \frac{h\sqrt{\alpha t}}{k} \right) \right] \operatorname{erfc} \left(\frac{x}{2\sqrt{\alpha t}} + \frac{h\sqrt{\alpha t}}{k} \right)$$

where x is the distance into the solid from the surface, erfc is the complimentary error function

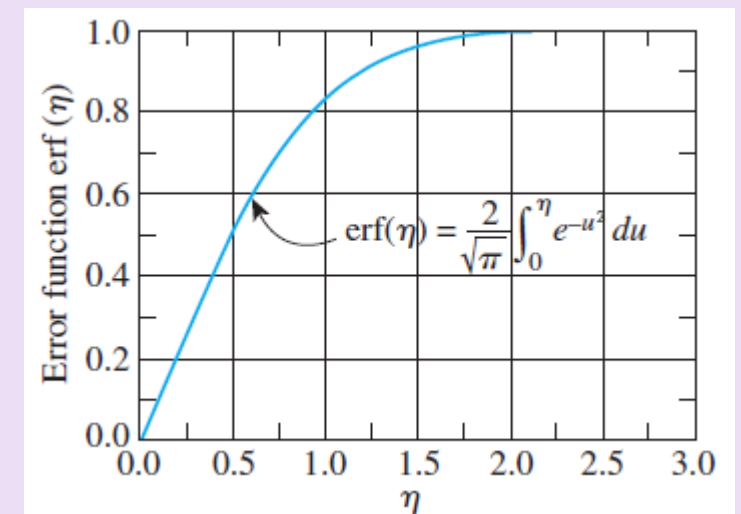
The function $\operatorname{erfc} = (1 - \operatorname{erf})$ where erf is the error function

Numerical values of the error function are available in standard text books

(samples are shown in the next slide)

$$\operatorname{erf}(z) = \frac{2}{\sqrt{\pi}} \int_0^z e^{-t^2} dt$$

Error function is a standard mathematical function, just like the sinus and tangent functions, whose value varies between 0 and 1.



Error function

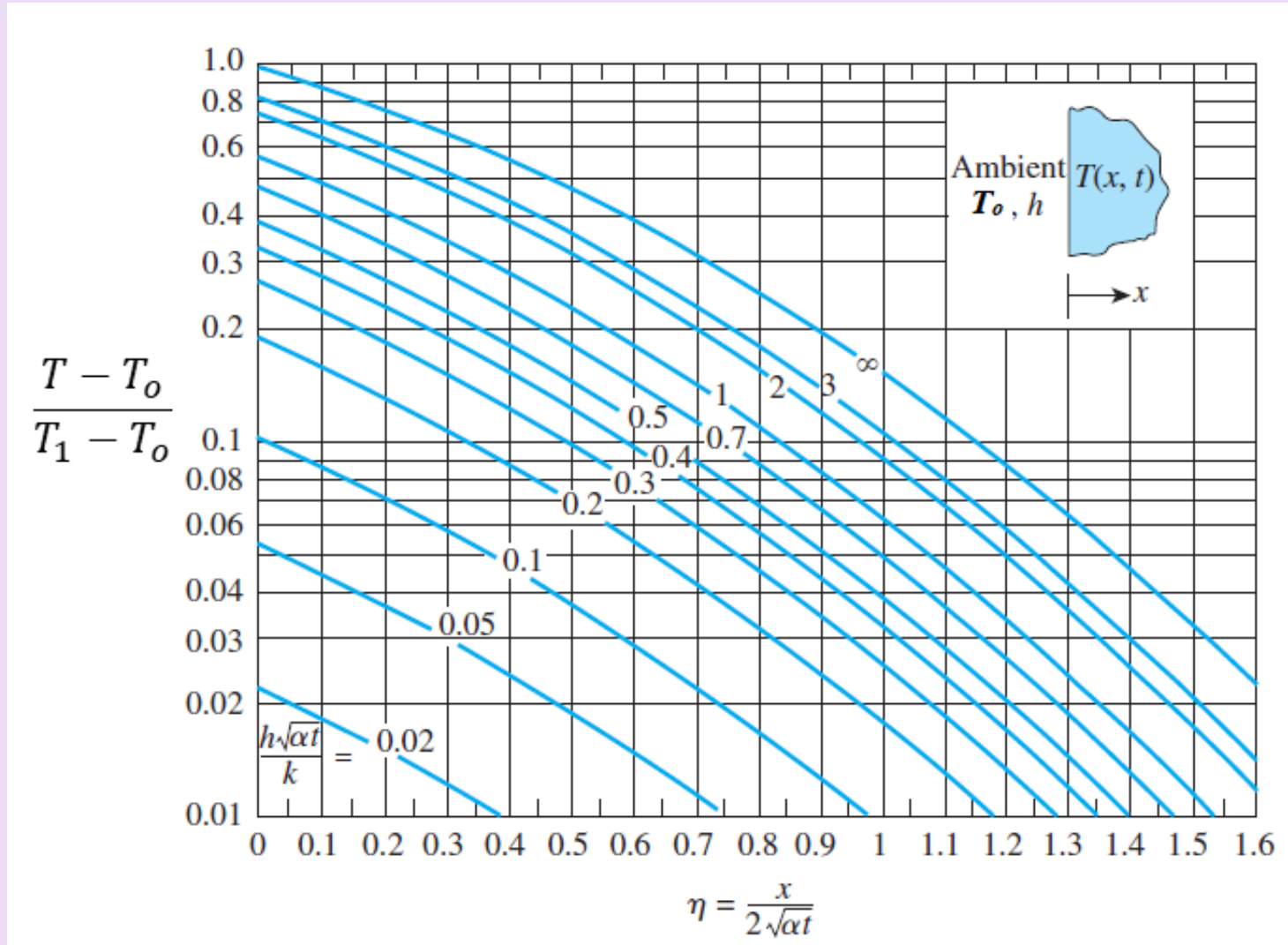
Numerical Values of Error Function $\text{erf}(z) = \frac{2}{\sqrt{\pi}} \int_{z=0}^z e^{-\xi^2} d\xi$

| z | erf z | z | erf z | z | erf z | z | erf z | z | erf z |
|------|---------|------|---------|------|---------|------|---------|------|---------|
| 0.00 | 0.00000 | 0.50 | 0.52049 | 1.00 | 0.84270 | 1.50 | 0.96610 | 2.00 | 0.99532 |
| 0.01 | 0.01128 | 0.51 | 0.52924 | 1.01 | 0.84681 | 1.51 | 0.96727 | 2.20 | 0.99814 |
| 0.02 | 0.02256 | 0.52 | 0.53789 | 1.02 | 0.85083 | 1.52 | 0.96841 | 2.40 | 0.99931 |
| 0.03 | 0.03384 | 0.53 | 0.54646 | 1.03 | 0.85478 | 1.53 | 0.96951 | 2.60 | 0.99976 |
| 0.04 | 0.04511 | 0.54 | 0.55493 | 1.04 | 0.85864 | 1.54 | 0.97058 | 2.80 | 0.99992 |
| 0.05 | 0.05637 | 0.55 | 0.56332 | 1.05 | 0.86243 | 1.55 | 0.97162 | 3.00 | 0.99998 |
| 0.06 | 0.06762 | 0.56 | 0.57161 | 1.06 | 0.86614 | 1.56 | 0.97262 | | |
| 0.07 | 0.07885 | 0.57 | 0.57981 | 1.07 | 0.86977 | 1.57 | 0.97360 | | |
| 0.08 | 0.09007 | 0.58 | 0.58792 | 1.08 | 0.87332 | 1.58 | 0.97454 | | |
| 0.09 | 0.10128 | 0.59 | 0.59593 | 1.09 | 0.87680 | 1.59 | 0.97546 | | |
| 0.10 | 0.11246 | 0.60 | 0.60385 | 1.10 | 0.88020 | 1.60 | 0.97634 | | |
| 0.11 | 0.12362 | 0.61 | 0.61168 | 1.11 | 0.88353 | 1.61 | 0.97720 | | |
| 0.12 | 0.13475 | 0.62 | 0.61941 | 1.12 | 0.88678 | 1.62 | 0.97803 | | |
| 0.13 | 0.14586 | 0.63 | 0.62704 | 1.13 | 0.88997 | 1.63 | 0.97884 | | |
| 0.14 | 0.15694 | 0.64 | 0.63458 | 1.14 | 0.89308 | 1.64 | 0.97962 | | |
| 0.15 | 0.16799 | 0.65 | 0.64202 | 1.15 | 0.89612 | 1.65 | 0.98037 | | |
| 0.16 | 0.17901 | 0.66 | 0.64937 | 1.16 | 0.89909 | 1.66 | 0.98110 | | |
| 0.17 | 0.18999 | 0.67 | 0.65662 | 1.17 | 0.90200 | 1.67 | 0.98181 | | |
| 0.18 | 0.20093 | 0.68 | 0.66378 | 1.18 | 0.90483 | 1.68 | 0.98249 | | |
| 0.19 | 0.21183 | 0.69 | 0.67084 | 1.19 | 0.90760 | 1.69 | 0.98315 | | |

The complementary error function

| η | erfc (η) | η | erfc (η) | η | erfc (η) |
|--------|-----------------|--------|-----------------|--------|-----------------|
| 0.00 | 1.00000 | 0.38 | 0.5910 | 0.76 | 0.2825 |
| 0.02 | 0.9774 | 0.40 | 0.5716 | 0.78 | 0.2700 |
| 0.04 | 0.9549 | 0.42 | 0.5525 | 0.80 | 0.2579 |
| 0.06 | 0.9324 | 0.44 | 0.5338 | 0.82 | 0.2462 |
| 0.08 | 0.9099 | 0.46 | 0.5153 | 0.84 | 0.2349 |
| 0.10 | 0.8875 | 0.48 | 0.4973 | 0.86 | 0.2239 |
| 0.12 | 0.8652 | 0.50 | 0.4795 | 0.88 | 0.2133 |
| 0.14 | 0.8431 | 0.52 | 0.4621 | 0.90 | 0.2031 |
| 0.16 | 0.8210 | 0.54 | 0.4451 | 0.92 | 0.1932 |
| 0.18 | 0.7991 | 0.56 | 0.4284 | 0.94 | 0.1837 |
| 0.20 | 0.7773 | 0.58 | 0.4121 | 0.96 | 0.1746 |
| 0.22 | 0.7557 | 0.60 | 0.3961 | 0.98 | 0.1658 |
| 0.24 | 0.7343 | 0.62 | 0.3806 | 1.00 | 0.1573 |
| 0.26 | 0.7131 | 0.64 | 0.3654 | 1.02 | 0.1492 |
| 0.28 | 0.6921 | 0.66 | 0.3506 | 1.04 | 0.1413 |
| 0.30 | 0.6714 | 0.68 | 0.3362 | 1.06 | 0.1339 |
| 0.32 | 0.6509 | 0.70 | 0.3222 | 1.08 | 0.1267 |
| 0.34 | 0.6306 | 0.72 | 0.3086 | 1.10 | 0.1198 |
| 0.36 | 0.6107 | 0.74 | 0.2953 | 1.12 | 0.1132 |

- The equation for solving the temperature at a particular x and t in case of unsteady state heat conduction for a semi-infinite solid is plotted in the form of a figure



Problem

The depth in the soil of the earth at which freezing temperatures penetrate is often of importance in agriculture and construction. During a certain fall day, the temperature in the earth is constant at 15.6°C to a depth of several metres. A cold wave suddenly reduces the air temperature from 15.6°C to -17.8°C . The convective coefficient above the soil is $11.36 \text{ W/m}^2\text{K}$. The soil properties can be assumed as $\alpha = 4.65 \times 10^{-7} \text{ m}^2/\text{s}$ and $k = 0.865 \text{ W/mK}$

- (a) What is the surface temperature after 5 h?
- (b) To what depth in the soil will the freezing temperature of 0°C penetrate in 5 h?

This is a case of unsteady state condition in a semi-infinite solid

For part (a) the value of x which is the distance from the surface, $x = 0$

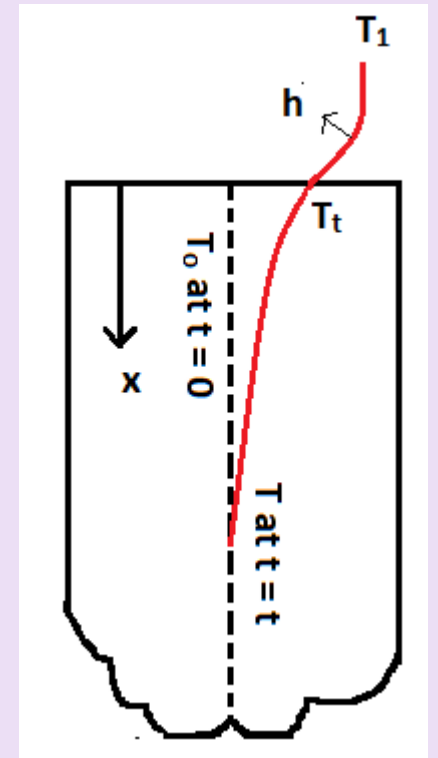
$$\text{The value of } \frac{x}{2\sqrt{\alpha t}} = \frac{0}{2 \times \sqrt{4.65 \times 10^{-7} \times 5 \times 3600}} = 0 \text{ and } \frac{h\sqrt{\alpha t}}{k} = \frac{11.36 \sqrt{4.65 \times 10^{-7} \times 5 \times 3600}}{0.865} = 1.2$$

$$\text{From the Figure at } \frac{x}{2\sqrt{\alpha t}} = 0 \text{ and } \frac{h\sqrt{\alpha t}}{k} = 1.2, \quad \frac{T - T_0}{T_1 - T_0} = 0.63$$

$$T_0 = 15.6 + 273 = 288.6 \text{ K}$$

$$\text{and } T_1 = -17.8 + 273 = 255.2 \text{ K}$$

$$T = 288.6 + 0.63(255.2 - 288.6) = 267.76 \text{ K or } -5.44^{\circ}\text{C}$$



For part (b) the temperature at a certain depth of x is $T = 273\text{ K}$ or 0°C

$$\frac{T - T_o}{T_1 - T_o} = \frac{273 - 288.6}{255.2 - 288.6} = 0.467$$

$$\text{Now } \frac{h\sqrt{\alpha t}}{k} = \frac{11.36\sqrt{4.65 \times 10^{-7} \times 5 \times 3600}}{0.865} = 1.2$$

From the Figure at $\frac{T - T_o}{T_1 - T_o} = 0.467$

and $\frac{h\sqrt{\alpha t}}{k} = 1.2$, it is seen that $\frac{x}{2\sqrt{\alpha t}} = 0.16$

Therefore,

$$x = 0.16 \times 2\sqrt{4.65 \times 10^{-7} \times 5 \times 3600}$$

$$x = 0.0293\text{ m}$$

