

**Mass Transfer: Concept of Fick's**  
**law of diffusion**

**MSE-S405**  
**(Heat and Mass Transfer)**

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# Fick's Law of Diffusion

Diffusion velocity  $\rightarrow$  During the diffusion process, the motion of various species takes place with respect to bulk or avg. velocity of the mix<sup>r</sup>. By this concept we can define mass diffusion & molar diffusion velocities based on avg. velocities —

① Mass diffusion velocity —

Mass diffusion velocity of component, A =  $u_A - u_{\text{mass}}$

\_\_\_\_\_ , B =  $u_B - u_{\text{mass}}$

② Molar diffusion velocity —

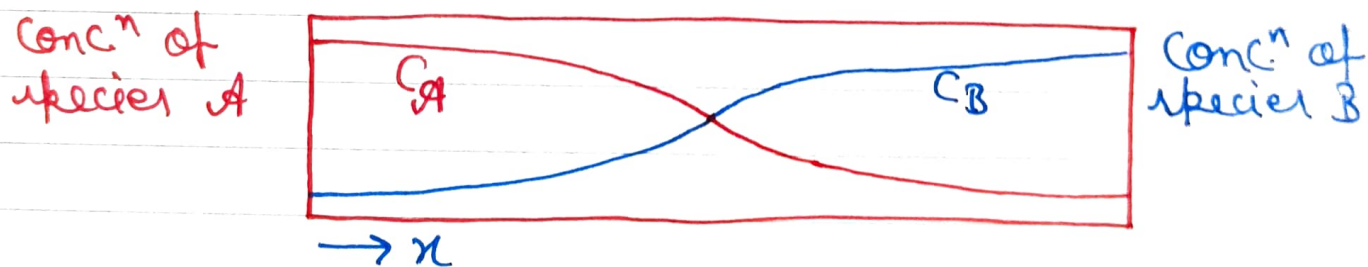
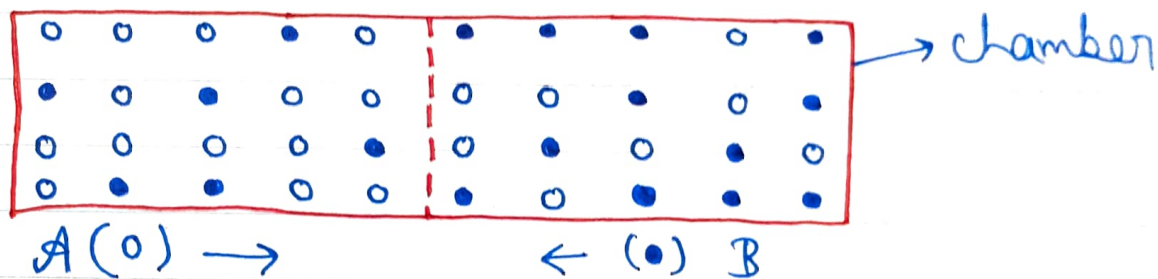
Molar diffusion velocity of component, A =  $u_A - u_{\text{molar}}$

\_\_\_\_\_ , B =  $u_B - u_{\text{molar}}$

FICK'S LAW  $\rightarrow$

In order to understand the mass diffusion (transport process), consider a chamber in which two different gases A & B, at the same temp. & pressure are initially separated by a partition. The left one has a high conc<sup>n</sup> (more molecules/area) of gas A whereas the right compartment

is rich in gas B, when the partition wall is removed a driving potential comes into existence which tends to equalize the conc<sup>n</sup> diff<sup>ce</sup>. Mass transfer by diffusion will be in the dir<sup>n</sup> of dec<sup>d</sup> conc<sup>n</sup> & subsequently there will be a net transport of species A to the right & of species B to the left. After a sufficient long period, equi<sup>m</sup> condi<sup>n</sup> prevail i.e., uniform conc<sup>n</sup> of species A & B are achieved & then the mass diffusion ceases.



It has been observed through experiments that molecular diffusion is governed by Fick's law, which is expressed as —

$$N_A = \frac{m_A}{A} = -D_{AB} \frac{dC_A}{dx}$$

$N_A \rightarrow$  mass flux of A i.e., amount of species A that is transferred per unit time & per unit area  $d^2$  to the dir<sup>n</sup> of transfer, ~~Kg~~ ( $\text{Kg/s-m}^2$  or  $\text{Kg mole/s-m}^2$ )

$m_A \rightarrow$  Mass flow rate of species A by diffusion ( $\text{Kg/s}$ )

$A \rightarrow$  Area through which mass is flowing ( $\text{m}^2$ )

$D_{AB} \rightarrow$  Diffusion coeff<sup>t</sup> or mass diffusivity for binary mix<sup>r</sup> of species A + B ( $\text{m}^2/\text{s}$ ).

$C_A \rightarrow$  conc<sup>n</sup> or molecules per unit vol.<sup>m</sup> of species A ( $\text{Kg/m}^3$ )

$\frac{dC_A}{dx} \rightarrow$  conc<sup>n</sup> of gradient of A, this acts as driving potential ( ~~$\text{Kg/m}$~~ )

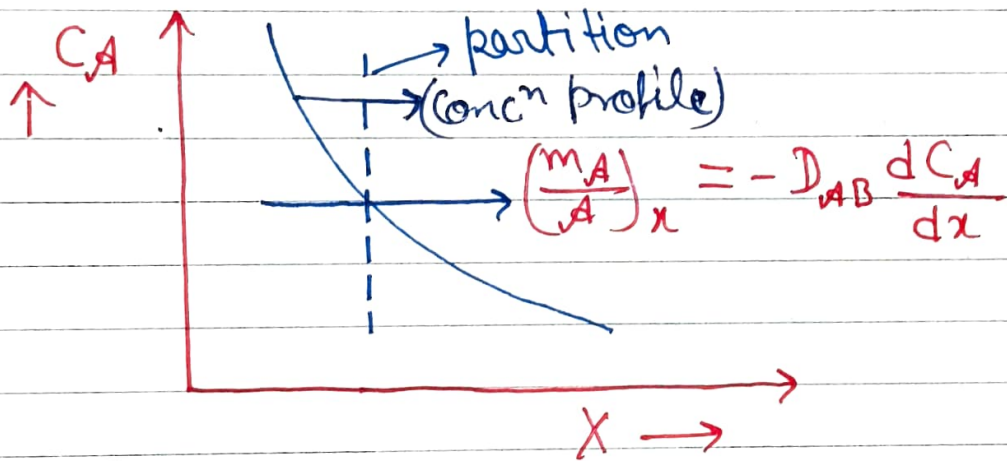
-ive  $\rightarrow$  -ive sign indicates that diffusion takes place in the dir<sup>n</sup> opposite to that of inc<sup>g</sup> conc<sup>n</sup>

The diffusion rate for B is —

$$\left\{ N_B = \frac{m_B}{A} = -D_{BA} \frac{dC_B}{dx} \right\}$$

It may be noted that diffusion coeff<sup>n</sup> i.e.,  $D_{AB}$  or  $D_{BA}$ , is independent upon the temp<sup>n</sup>, pressure & nature of the components of the syst.

### Physical mechanism of diffusion →



We observe that the conc<sup>n</sup> of species A (moles/vol<sup>m</sup>) on left of partition is much greater than the conc<sup>n</sup> of species A on the right side of the partition. ∴, the more molecules of A cross the plane per unit time from left to right than in the opposite direction. It results into the net mass transfer of A from high conc<sup>n</sup> region to low conc<sup>n</sup> region till the equilibrium established.



Q: A steel rectangular container having walls 16 mm thick is used to store gaseous hydrogen at elevated pressure. The molar concentrations of hydrogen in the steel at the inside & outside surfaces are  $1.2 \text{ Kg-mole/m}^3$  & zero respectively. Assuming the diffusion coeff<sup>t</sup> for hydrogen in steel as  $0.248 \times 10^{-12} \text{ m}^2/\text{s}$ , then calculate the molar diffusion flux for hydrogen through the steel.

$$A: N_A = D_A \frac{(C_{A1} - C_{A2})}{L}$$

$$\Rightarrow N_A = 0.248 \times 10^{-12} \times \frac{(1.2 - 0)}{0.016}$$

$$\Rightarrow N_A = 1.86 \times 10^{-11} \frac{\text{Kg-mole}}{\text{m}^2\text{-sec.}}$$

← Ans